

Relay Feedback Based Time Domain Modeling of Linear 3-by-3 MIMO System

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Abstract Relay feedback tests are carried out on multi input multi output systems. Analytical expressions for relay responses in time domain for the interactive transfer functions (off-diagonal elements) of the systems are derived and are validated. Generalized expressions are formulated based on the observation that a relay feedback test consists of a series of step inputs and a stable limit cycle implies a convergent infinite series. MIMO systems with lower-order transfer functions with different time delays are used to illustrate the derivation. These analytical expressions, in a closed form solution are useful to identify unknown system parameters, to understand interactions, to diagnosis the fault at the earlier stage, and subsequently for auto tuning. This closed-loop equation not only enables us to assess the effect of interactions between inputs and outputs but is also useful to back calculate/estimate the exact process model parameters, appearing in the analytical expressions for linear 3-by-3 MIMO systems, from experimental response.

Keywords Modelling, Relay Feedback, Identification, Auto Tuning, Multi Input Multi Output

1. Introduction

Chemical processes are complex and non-linear in nature due to interactions (Seborg et. al, 2004) between inputs and outputs. With increase in complexity of the process, it becomes difficult to control the loops properly. Whenever closed loop performance degrades, loops must be retuned with correct input-output pairs. The sequential identification and the expert controller design methods form the basic structure for the multivariable autotuner that allows loop tuning without breaking the loop and without interrupting production, in process industries.

The relay feedback test was first proposed by Astrom and Hagglund (1984) for process control practitioners as a closed-loop tool for system identification and control. In this method (Astrom and Hagglund, 1984), periodic step functions are given as input to the unknown process and outputs are collected (that lags behind input by π radians) from which limit cycle data (Ku and Wu) are found to approximate the process model parameters. Many researchers (Luyben, 1987; Yu, 1999; Majhi and Atherton, 1999; Wang et.al., 1997) have worked on autotuning of PID controller for low order systems and have reported of getting more information and better performance of closed-loop system. Reports have also been presented on formulating mathematical models (Thyagarajan & Yu, 2002; Panda & Yu, 2003; Lee &

Edgar, 2007; Liu & Gao, 2008) in time domain for relay responses for identifying process parameters. But these processes are based on single input single output where there is no interaction between input and output. As chemical systems are dominated in time delay and most of them are multivariable in nature, Shen & Yu (1994) and Wang et.al (1997) presented relay feedback based parameter estimation methods for MIMO systems. Palmor et.al.(1995) and Wang et.al. (2000) discussed stability of limit cycles in decentralized MIMO systems. These methods consider desired response (output: for example y_1 in case of 2x2 system) and input (u_1) for system identification and analysis and they do not discuss about methods to reduce interactions nor do they give any exact analytical expressions for the relay responses that may help in analyzing the interaction behaviour between input/output and may provide information regarding closed-loop parameters of the MIMO system. Moreover, it has been felt that exact model parameters and information on interactions can be better obtained / calculated from mathematical model of relay responses for MIMO systems. As the off-diagonal closedloop transfer functions contain information on interactions, it is better to analyze the control system based on their time domain characteristics. With this objective in mind, time domain expressions of relay responses for interactive transfer functions are developed in this article. Relay tests are carried out on MIMO processes (2x2 and 3x3 systems with square matrix structures and transfer functions of FOPDT type) and undesirable responses are modeled. Recently some more researchers[12-15] have presented time domain models for relay responses of SISO systems but the above problem remained unaddressed.

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This paper is organized as follows: introduction to relay feedback test on MIMO process was detailed in section 2 followed by general description of typical 3x3 multivariable processes. In section 4, modeling equations for relay responses of 3x3 processes are developed. Analytical expressions thus obtained, are validated in section 5 for relay feedback responses through modeling in order to characterize the undesired responses. The simulation results on some 3x3 processes are characterized in section 6. Concluding remarks are drawn in the final section.

2. Relay Feedback Test on MIMO Process

Based on the concept of sequential auto tuning (Shen & Yu,[8]) method each controller is designed in sequence. Let's consider a 3-by-3 MIMO system with a known pairing $(y_1 - u_1)$, $(y_2 - u_2)$ and $(y_3 - u_3)$ under decentralized PI control (Figure 1). Initially, an ideal relay is placed between y_1 and u_1 , while loop 2 and loop 3 is on manual. Following the relay-feedback test, a controller can be designed from the ultimate gain and ultimate frequency. The next step is to perform relay-feedback test between y_2 and u_2 while loop 1 is on automatic and loop 3 is on manual. Finally, relay-feedback test between y_3 and u_3 while loop 1 and loop 2 is on automatic, a controller can also be designed for loop 3 following the relay-feedback test. This procedure is repeated until the controller parameters converge. Typically, the controller parameters converge in 3 - 4 relay-feedback tests for 3-by-3 MIMO systems.

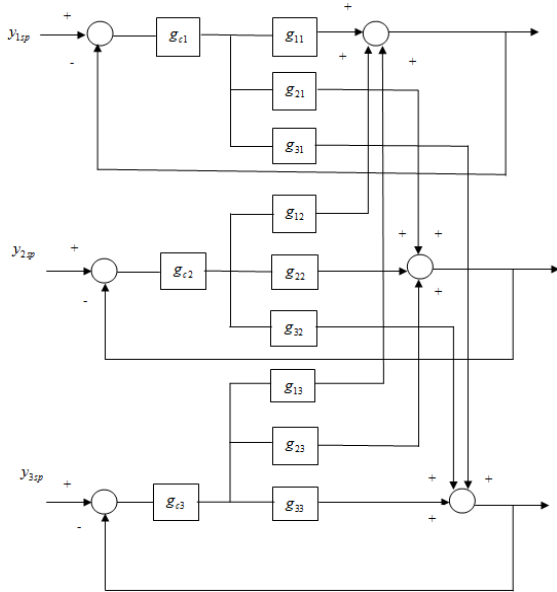


Figure 1. Closed loop representation of 3-by-3 MIMO process with decentralized control structure

The 3-by-3 MIMO process with decentralized control structure is shown in Figure. 2. For 3-by-3 MIMO system, described by Eq. (2.1) as

$$\begin{pmatrix} y_1 \\ y_2 \\ y_3 \end{pmatrix} = \begin{pmatrix} g_{11} & g_{12} & g_{13} \\ g_{21} & g_{22} & g_{23} \\ g_{31} & g_{32} & g_{33} \end{pmatrix} \begin{pmatrix} u_1 \\ u_2 \\ u_3 \end{pmatrix} \quad (2.1)$$

The decentralized controller is described by Eq. (2.2) as

$$G_c(s) = \begin{pmatrix} G_{c1} & 0 & 0 \\ 0 & G_{c2} & 0 \\ 0 & 0 & G_{c3} \end{pmatrix} \quad (2.2)$$

As it is evident from closed-loop sequential auto tuning, for a 3-by-3 system, we come across $G_{11,CL}$, $G_{22,CL}$ and $G_{33,CL}$ as diagonalised transfer functions (that govern basic transfer functions for controller design) and interactive transfer functions as $G_{12,CL}$, $G_{13,CL}$, $G_{21,CL}$, $G_{23,CL}$, $G_{31,CL}$ and $G_{32,CL}$.

The effective closed loop relation between y_2 and u_1 for 3-by-3 MIMO system is

$$G_{21,CL} = \frac{g_{21}}{1 + G_{c2}g_{22}} - \frac{g_{23}g_{31}}{G_{c3}g_{33}(1 + G_{c3}g_{33})} \quad (2.3)$$

$$g_{21} = \frac{k_{21}e^{-D_{21}s}}{\tau_{21}s + 1}; \quad g_{22} = \frac{k_{22}e^{-D_{22}s}}{\tau_{22}s + 1}; \quad g_{23} = \frac{k_{23}e^{-D_{23}s}}{\tau_{23}s + 1};$$

$$g_{31} = \frac{k_{31}e^{-D_{31}s}}{\tau_{31}s + 1}; \quad g_{33} = \frac{k_{33}e^{-D_{33}s}}{\tau_{33}s + 1};$$

$$G_{c2} = k_{c2} \left(1 + \frac{1}{\tau_{i2}s} \right)$$

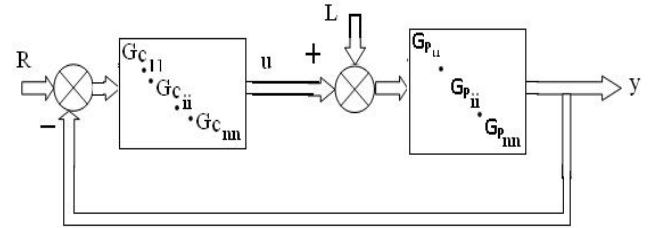


Figure 2. Block diagram of nxn multivariable systems with decentralized PI controller

3. Description of 2x2 System and 3x3 System

Let us consider squared MIMO systems of 2 x 2 and 3x3 types:

The interactive transfer functions for 2 x 2 and 3 x 3 system are g_{p12} and g_{p21} . The effective closed loop relation between y_2 and u_1 for 2x2 system is

$$g_{p21,cl} = \frac{g_{p21}}{1 + G_{c2}g_{p22}} \text{ where, } g_{p21} = \frac{k_{21}e^{-D_{21}s}}{\tau_{21}s + 1}$$

$$g_{p22} = \frac{k_{22}e^{-D_{22}s}}{\tau_{22}s + 1} \text{ and}$$

$$G_{c2} = k_{c2} \left(1 + \frac{1}{\tau_{i2}s} \right) \quad (3.1)$$

2x2 system	3x3 system
$g_p(s) = \begin{pmatrix} g_{p11} & g_{p12} \\ g_{p21} & g_{p22} \end{pmatrix}$ $G_c(s) = \begin{pmatrix} G_{c1} & 0 \\ 0 & G_{c2} \end{pmatrix}$ $u(s) = [u_1(s) \ u_2(s)]^T$ $y(s) = [y_1(s) \ y_2(s)]^T$	$g_p(s) = \begin{pmatrix} g_{p11} & g_{p12} & g_{p13} \\ g_{p21} & g_{p22} & g_{p23} \\ g_{p31} & g_{p32} & g_{p33} \end{pmatrix}$ $G_c(s) = \begin{pmatrix} G_{c1} & 0 & 0 \\ 0 & G_{c2} & 0 \\ 0 & 0 & G_{c3} \end{pmatrix}$ $u(s) = [u_1(s) \ u_2(s) \ u_3(s)]^T$ $y(s) = [y_1(s) \ y_2(s) \ y_3(s)]^T$
$g_{p21,cl} = \frac{g_{p21}}{1 + G_{c2}g_{p22}}$	$g_{p21,cl} = \frac{g_{p21}}{1 + G_{c2}g_{p22}} - \frac{g_{p23}g_{p31}}{G_{c3}g_{p33}(1 + G_{c3}g_{p33})}$

The effective closed loop relation between y_2 and u_1 for 3x3 system is

$$g_{p21,cl} = \frac{g_{p21}}{1 + G_{c2}g_{p22}} - \frac{g_{p23}g_{p31}}{G_{c3}g_{p33}(1 + G_{c3}g_{p33})}$$

$$g_{p31} = \frac{k_{31}e^{-D_{31}s}}{\tau_{31}s + 1} \quad g_{p23} = \frac{k_{23}e^{-D_{23}s}}{\tau_{23}s + 1} \quad G_{c2} = k_{c2} \left(1 + \frac{1}{\tau_{i2}s} \right) \quad (3.2)$$

4. Modeling of 2x2 and 3x3 System

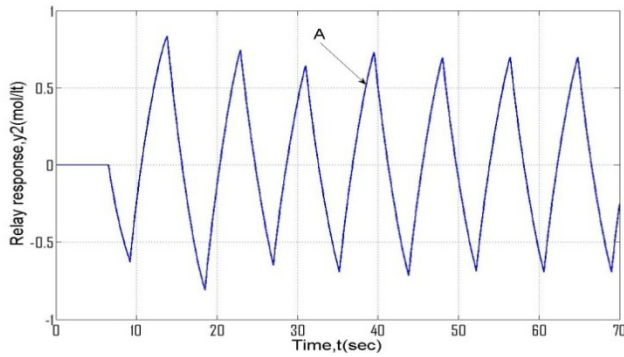


Figure 3a. Relay feedback response of 3x3 systems (OR distillation column)

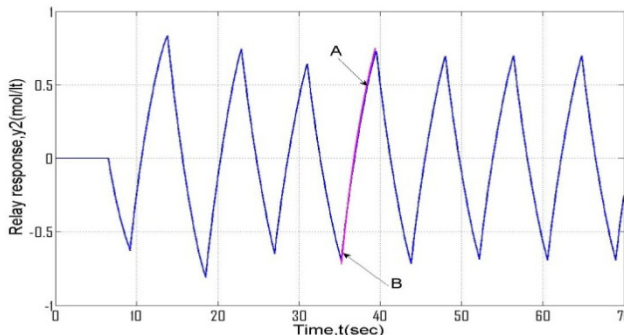


Figure 3b. Validation of analytical expression of 3x3 interactive cross TF with experimental relay response (OR column)

Mathematical models are developed to represent relay responses produced by closed loop interaction transfer function for 3 input 3 output systems (Eqn. 3.2). It is assumed that relay output is generated by a series of small number of step changes in manipulated variable. Hence the

stabilized output is a sum of infinite terms of small responses due to those step changes. The typical relay feedback response of closed loop interaction transfer function of 3x3 systems is shown in Figure 3a.

4.1. The Relay Response of 3x3 MIMO Systems

For 3x3 systems the relay responses obtained from interactive transfer functions are modeled as follows. The relay response is assumed to be formed by n-number of small step changes. At the first interval, the response can be described as

$$y_1 = \left(k_{21} \left[1 - e^{-t/\tau_{21}} \right] - \frac{k_{22}k_{c2}}{\tau_{i2}} \left[1 + (\tau_{i2} - \tau_{22}) e^{-t/\tau_{22}} \right] \right) - \quad (4.1)$$

$$\left(\frac{k_{23}k_{c3}\tau_{i3}}{k_{c3}k_{33}} \left[1 - \left(a_1 e^{-t/\tau_{i3}} + a_2 e^{-t/\tau_{23}} + a_3 e^{-t/\tau_{33}} \right) \right] - \frac{k_{33}k_{c3}}{\tau_{i3}} \left[1 + (\tau_{i3} - \tau_{33}) e^{-t/\tau_{33}} \right] \right)$$

Where

$$a_1 = \frac{\tau_{i3}(\tau_{i3} - \tau_{33})}{(\tau_{i3} - \tau_{23})(\tau_{i3} - \tau_{31})}; a_2 = \frac{\tau_{23}(\tau_{23} - \tau_{33})}{(\tau_{23} - \tau_{i3})(\tau_{23} - \tau_{31})}; a_3 = \frac{\tau_{31}(\tau_{31} - \tau_{33})}{(\tau_{31} - \tau_{i3})(\tau_{31} - \tau_{23})}$$

Let $D = D_{23} + D_{31} - D_{33}$, at the second instant, the relay output can be given by

$$y_2 = k_{21} \left[\left(1 - e^{-\frac{t+D_{21}}{\tau_{21}}} \right) - 2 \left(1 - e^{-\frac{t}{\tau_{21}}} \right) \right] - \frac{k_{22}k_{c2}}{\tau_{i2}} \left[\left(1 + (\tau_{i2} - \tau_{22}) e^{-\frac{t+D_{22}}{\tau_{22}}} \right) - 2 \left(1 + (\tau_{i2} - \tau_{22}) e^{-\frac{t}{\tau_{22}}} \right) \right] - \left(\frac{k_{23}k_{c3}\tau_{i3}}{k_{c3}k_{33}} \left[1 - \left(a_1 e^{-\frac{t+D}{\tau_{i3}}} + a_2 e^{-\frac{t+D}{\tau_{23}}} + a_3 e^{-\frac{t+D}{\tau_{31}}} \right) \right] - \frac{k_{33}k_{c3}}{\tau_{i3}} \left[1 + (\tau_{i3} - \tau_{33}) e^{-\frac{t+D_{33}}{\tau_{33}}} \right] - 2 \left(1 + (\tau_{i3} - \tau_{33}) e^{-\frac{t}{\tau_{33}}} \right) \right] \right) \quad (4.2)$$

The above equation (4.2) can be simplified as

$$y_2 = k_{21} \left\{ \left[1 - 2 \right] - e^{-\frac{t}{\tau_{21}}} \left[e^{\frac{D_{21}}{\tau_{21}}} - 2 \right] \right\} - \frac{k_{22}k_{c2}}{\tau_{i2}} \left\{ \left[1 - 2 \right] + \left(\tau_{i2} - \tau_{22} \right) e^{-\frac{t}{\tau_{22}}} \left[e^{\frac{D_{22}}{\tau_{22}}} - 2 \right] \right\} - \left(\frac{k_{23}k_{c3}\tau_{i3}}{k_{c3}k_{33}} \left[1 - \left(a_1 e^{-\frac{t}{\tau_{i3}}} \left[e^{\frac{D}{\tau_{i3}}} - 2 \right] + a_2 e^{-\frac{t}{\tau_{23}}} \left[e^{\frac{D}{\tau_{23}}} - 2 \right] + a_3 e^{-\frac{t}{\tau_{31}}} \left[e^{\frac{D}{\tau_{31}}} - 2 \right] \right) \right] - \frac{k_{33}k_{c3}}{\tau_{i3}} \left[1 - 2 \right] + \left(\tau_{i3} - \tau_{33} \right) e^{-\frac{t}{\tau_{33}}} \left[e^{\frac{D_{33}}{\tau_{33}}} - 2 \right] \right] \right\}$$

At the third instant,

$$y_3 = k_{21} \left[\left(1 - e^{-\frac{t+D_{21}+\frac{p_u}{2}}{\tau_{21}}} \right) - 2 \left(1 - e^{-\frac{t+D_{21}}{\tau_{21}}} \right) + 2 \left(1 - e^{-\frac{t}{\tau_{21}}} \right) \right] - \frac{k_{22}k_{c2}}{\tau_{i2}} \left[\left(1 + (\tau_{i2} - \tau_{22}) e^{-\frac{t+D_{22}+\frac{p_u}{2}}{\tau_{22}}} \right) - 2 \left(1 + (\tau_{i2} - \tau_{22}) e^{-\frac{t+D_{22}}{\tau_{22}}} \right) + 2 \left(1 + (\tau_{i2} - \tau_{22}) e^{-\frac{t}{\tau_{22}}} \right) \right] - \frac{k_{23}k_{c3}}{\tau_{i3}} \left[\left(1 + (\tau_{i3} - \tau_{33}) e^{-\frac{t+D_{33}+\frac{p_u}{2}}{\tau_{33}}} \right) - 2 \left(1 + (\tau_{i3} - \tau_{33}) e^{-\frac{t+D_{33}}{\tau_{33}}} \right) + 2 \left(1 + (\tau_{i3} - \tau_{33}) e^{-\frac{t}{\tau_{33}}} \right) \right] - \frac{k_{23}k_{31}\tau_{i3}}{k_{c3}k_{33}} \left[\left(1 - 2 \left(a_1 e^{-\frac{t+D}{\tau_{i3}}} + a_2 e^{-\frac{t+D}{\tau_{23}}} + a_3 e^{-\frac{t+D}{\tau_{31}}} \right) + 2 \left(a_1 e^{-\frac{t}{\tau_{i3}}} + a_2 e^{-\frac{t}{\tau_{23}}} + a_3 e^{-\frac{t}{\tau_{31}}} \right) \right) \right] - \frac{k_{33}k_{c3}}{\tau_{i3}} \left[\left(1 - 2 \left(a_1 e^{-\frac{t+D}{\tau_{i3}}} + a_2 e^{-\frac{t+D}{\tau_{23}}} + a_3 e^{-\frac{t+D}{\tau_{31}}} \right) + 2 \left(a_1 e^{-\frac{t}{\tau_{i3}}} + a_2 e^{-\frac{t}{\tau_{23}}} + a_3 e^{-\frac{t}{\tau_{31}}} \right) \right) \right] \quad (4.3)$$

This eq. (4.3) can be simplified as

$$y_3 = k_{21} \left\{ [1-2] - e^{-\frac{t}{\tau_{21}}} \left[e^{-\frac{D_{21}+\frac{p_u}{2}}{\tau_{21}}} - 2 * e^{-\frac{D_{21}}{\tau_{21}}} + 2 \right] \right\} - \frac{k_{22}k_{c2}}{\tau_{i2}} \left\{ [1-2] + \left((\tau_{i2} - \tau_{22}) e^{-\frac{t}{\tau_{22}}} \left[e^{-\frac{D_{22}+\frac{p_u}{2}}{\tau_{22}}} - 2 * e^{-\frac{D_{22}}{\tau_{22}}} + 2 \right] \right) \right\} - \frac{k_{23}k_{31}\tau_{i3}}{k_{c3}k_{33}} \left\{ 1 - \left(a_1 e^{-\frac{t}{\tau_{i3}}} \left[e^{-\frac{D+\frac{p_u}{2}}{\tau_{i3}}} - 2 * e^{-\frac{D}{\tau_{i3}}} - 2 \right] + a_2 e^{-\frac{t}{\tau_{23}}} \left[e^{-\frac{D+\frac{p_u}{2}}{\tau_{23}}} - 2 * e^{-\frac{D}{\tau_{23}}} - 2 \right] + a_3 e^{-\frac{t}{\tau_{31}}} \left[e^{-\frac{D+\frac{p_u}{2}}{\tau_{31}}} - 2 * e^{-\frac{D}{\tau_{31}}} - 2 \right] \right) \right\} - \frac{k_{33}k_{c3}}{\tau_{i3}} \left\{ [1-2] + \left((\tau_{i3} - \tau_{33}) e^{-\frac{t}{\tau_{33}}} \left[e^{-\frac{D_{33}+\frac{p_u}{2}}{\tau_{33}}} - 2 * e^{-\frac{D_{33}}{\tau_{33}}} - 2 \right] \right) \right\}$$

As time tends to infinity, the response becomes stabilized.

Thus, the overall response can be described as

$$y_t = k_{21} \left\{ [1-2+2-.....] - e^{-\frac{t}{\tau_{21}}} \left[e^{-\frac{D_{21}+\sum_{n=1}^{n-1} \frac{p_u}{2}}{\tau_{21}}} - 2e^{-\frac{D_{21}}{\tau_{21}}} + + 2e^{-\frac{p_u}{2\tau_{21}}} - 2 \right] \right\} -$$

$$- \frac{k_{22}k_{c2}}{\tau_{i2}} \left\{ [1-2+2-.....] + \left((\tau_{i2} - \tau_{22}) e^{-\frac{t}{\tau_{22}}} \left[e^{-\frac{D_{22}+\sum_{n=1}^{n-1} \frac{p_u}{2}}{\tau_{22}}} - 2e^{-\frac{D_{22}}{\tau_{22}}} + + 2e^{-\frac{p_u}{2\tau_{22}}} - 2 \right] \right) \right\} - \frac{k_{23}k_{31}\tau_{i3}}{k_{c3}k_{33}} \left\{ 1 - \left(a_1 e^{-\frac{t}{\tau_{i3}}} \left[e^{-\frac{D+\sum_{n=1}^{n-1} \frac{p_u}{2}}{\tau_{i3}}} - 2 * e^{-\frac{D}{\tau_{i3}}} + 2 * e^{-\frac{p_u}{2\tau_{i3}}} - 2 \right] + a_2 e^{-\frac{t}{\tau_{23}}} \left[e^{-\frac{D+\sum_{n=1}^{n-1} \frac{p_u}{2}}{\tau_{23}}} - 2 * e^{-\frac{D}{\tau_{23}}} + 2 * e^{-\frac{p_u}{2\tau_{23}}} - 2 \right] + a_3 e^{-\frac{t}{\tau_{31}}} \left[e^{-\frac{D+\sum_{n=1}^{n-1} \frac{p_u}{2}}{\tau_{31}}} - 2 * e^{-\frac{D}{\tau_{31}}} + 2 * e^{-\frac{p_u}{2\tau_{31}}} - 2 \right] \right) \right\} - \frac{k_{33}k_{c3}}{\tau_{i3}} \left\{ [1-2] + \left((\tau_{i3} - \tau_{33}) e^{-\frac{t}{\tau_{33}}} \left[e^{-\frac{D_{33}+\sum_{n=1}^{n-1} \frac{p_u}{2}}{\tau_{33}}} - 2 * e^{-\frac{D_{33}}{\tau_{33}}} + 2 * e^{-\frac{p_u}{2\tau_{33}}} - 2 \right] \right) \right\} \quad (4.4)$$

The above eq (4.4) can be written as

$$y_t = k_{21} \{ \text{firstpart} - \text{secondpart} \} - \frac{k_{22}k_{c2}}{\tau_{i2}} \{ \text{thirdpart} + \text{fourthpart} \} - \frac{k_{23}k_{31}\tau_{i3}}{k_{c3}k_{33}} \{ 1 - (\text{fifthpart} + \text{sixthpart} + \text{seventhpart}) \} - \frac{k_{33}k_{c3}}{\tau_{i3}} \{ \text{eighthpart} + \text{ninthpart} \}$$

Let $r_1 = e^{-\frac{p_u}{2\tau_{21}}}$; $r_2 = e^{-\frac{p_u}{2\tau_{22}}}$; $r_3 = e^{-\frac{p_u}{2\tau_{i3}}}$; $r_4 = e^{-\frac{p_u}{2\tau_{23}}}$ and $r_5 = e^{-\frac{p_u}{2\tau_{33}}}$

The RHS of the above series becomes

First part = $[1-2+2-.....] = 1$

In similar way, third part = 1

Secondpart = $2 \left[e^{-\frac{D_{21}}{\tau_{21}}} r_1^n - 2r_1^{n-1} + 2r_1^{n-2} - + 2r_1 - 2 \right]$ This second

part can be put into following series

$$\text{thirdpart} = 2 \left[1 - r_1 + r_1^2 - r_1^3 + ... \right] = \frac{2}{1+r_1} = \frac{2}{1+e^{-\frac{p_u}{2\tau_{21}}}}$$

In similar way, fourthpart = $\frac{2}{1+r_2} = \frac{2}{1+e^{-\frac{p_u}{2\tau_{22}}}}$

$$\text{fifthpart} = \frac{2}{1+r_3} = \frac{2}{1+e^{-\frac{p_u}{2\tau_{i3}}}}; \text{sixthpart} = \frac{2}{1+r_4} = \frac{2}{1+e^{-\frac{p_u}{2\tau_{23}}}};$$

$$\text{seventhpart} = \frac{2}{1+r_5} = \frac{2}{1+e^{-\frac{p_u}{2\tau_{33}}}}$$

The generalized analytical expressions for 3x3 system is given by

$$y_n = k_{21} \left(1 - e^{-\frac{t}{\tau_{21}}} \left(\frac{2}{1+e^{-\frac{p_u}{2\tau_{21}}}} \right) \right) - \frac{k_{22}k_{e2}}{\tau_{12}} \left(1 + (\tau_{12} - \tau_{22}) e^{-\frac{t}{\tau_{22}}} \left(\frac{2}{1+e^{-\frac{p_u}{2\tau_{21}}}} \right) \right) - \left[1 - \left(a_1 e^{-\frac{t}{\tau_{13}}} \left(\frac{2}{1+e^{-\frac{p_u}{2\tau_{13}}}} \right) + a_2 e^{-\frac{t}{\tau_{23}}} \left(\frac{2}{1+e^{-\frac{p_u}{2\tau_{23}}}} \right) + a_3 e^{-\frac{t}{\tau_{33}}} \left(\frac{2}{1+e^{-\frac{p_u}{2\tau_{33}}}} \right) \right) \right] - \left[\frac{k_{33}k_{e3}}{\tau_{13}} \left(1 + (\tau_{13} - \tau_{33}) e^{-\frac{t}{\tau_{33}}} \left(\frac{2}{1+e^{-\frac{p_u}{2\tau_{33}}}} \right) \right) \right] \quad (4.5)$$

after normalizing $\frac{k_{23}k_{31}\tau_{13}}{k_{e3}k_{33}}$ to unity and assuming $y(t-D_{22})=1$; $y(t-D_{33})=1$, eq. (4.5) can be simulated and Figure 3b and Figure 4a can be generated.

5. Validation of Analytical Expressions for 2x2 and 3x3 Systems

The transfer function of Ogunike & Ray (OR) distillation column is given by

$$\begin{bmatrix} y_1 \\ y_2 \\ y_3 \end{bmatrix} = \begin{bmatrix} \frac{0.66e^{-2.6s}}{6.7s+1} & \frac{-0.61e^{-3.5s}}{8.64s+1} & \frac{-0.0049e^{-s}}{9.06s+1} \\ \frac{-2.36e^{-3s}}{5s+1} & \frac{-2.3e^{-3s}}{5s+1} & \frac{-0.01e^{-1.2s}}{7.09s+1} \\ \frac{-34.68e^{-9.2s}}{8.15s+1} & \frac{46.2e^{-9.4s}}{10.9s+1} & \frac{0.87(11.61s+1)e^{-s}}{(3.89s+1)(18.8s+1)} \end{bmatrix} \begin{bmatrix} u_1 \\ u_2 \\ u_3 \end{bmatrix} \quad (5.1)$$

The above transfer function represents multiproduct plant distillation column for the separation of binary mixture of ethanol-water (Ogunnaik-Ray (OR) column). The top compositions (y) are controlled by manipulating the reflux (V) and the reboiler steam flow rates and pressure. Feed flow rate (F) is disturbance. It can be noted that gp33(s) can be approximated to FOPDT model structure (Skogestad, 2003) after which relay response can be generated using simulink (experimental). Responses obtained after simulating OR column (in simulink) are compared with its original relay responses (obtained by simulating Eq. 4.5). Figure 3b and Figure 4a show the validation of derived mathematical models where theoretical response matches exactly with simulated (simulink platform) one. Figure 3b shows interactive transfer function of OR columns. AB is response of theoretical equation while the other continuous curve is generated from experiment. Figure 4a presents validation of one-loop of interactive transfer function of 3x3 column OR system under measurement noise. Figure 4b shows the validation of undesired-relay feedback responses for

real-time liquid level system.

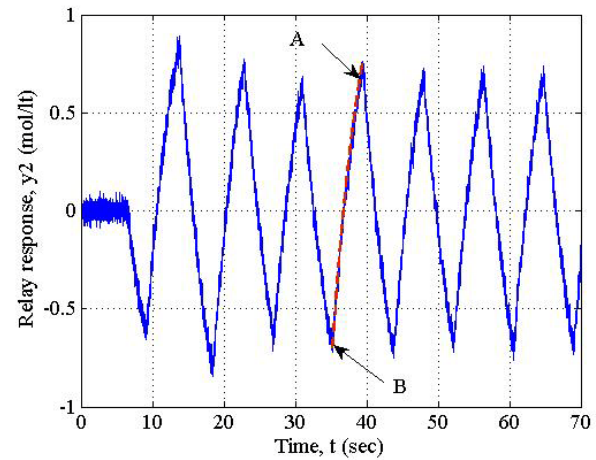


Figure 4a. Validation of analytical expression (AB) of 3x3 interactive cross TF with experimental relay response in the presence of measurement noise (OR column)

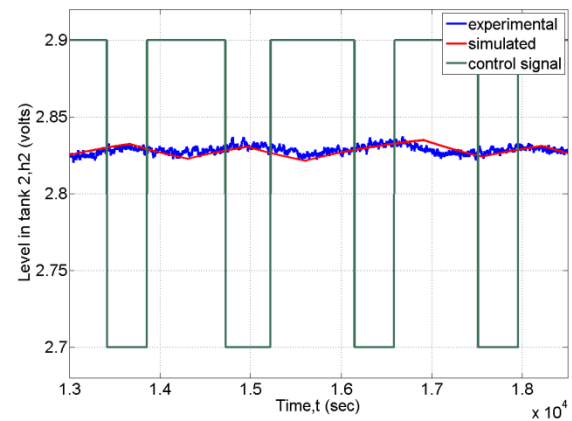


Figure 4b. Validation of analytical expression (smooth) of 2x2 interactive cross TF with real time experimental relay response (noisy) in the presence of measurement noise (Liq level system)

Experimental setup: The coupled tanks set-up is a model of a liquid storage system in process industries. Often tanks are coupled through connecting pipes. These storage facilities contain fluids where the reactant level and flow are to be controlled. Water is chosen as the fluid. The experiment set-up of coupled tanks is designed so that the system can be configured. The set-up has four translucent tanks each with a pressure sensor to measure the water levels. The couplings between the tanks can be modified by the use of seven manual valves to change the dynamics of the system imposing the use of different controllers. Water is delivered to the tanks by two independently controlled, submersed pumps. Step disturbances on the flowrate are provided by four manual valves. Drain flow rates can be modified using orifice caps that are easy to change. The 33-041 coupled tank system is interfaced with computer through MATLAB / SIMULINK and an Advantech PCI 1711 data acquisition interface card.

The schematic of the coupled tanks experimental system

as shown in Figure 5 has been used to control the levels in the lower two tanks with two pumps. The process inputs are u_1 and u_2 (input voltages to excite the pumps) and the outputs are h_4 and h_2 (heights from level measurement devices). The design parameters of the coupled tanks experimental set up are cross-sectional area of each tank, $A=0.01389\text{m}^2$; outlet (exit pipe) area of tank, $a=50.2658\times 10^{-6}\text{m}^2$ and gravitational constant, $g=9.81\text{ m/s}^2$. A step disturbance on u_1 is given and changes in h_4 and h_2 are recorded. Similar step responses in levels for step disturbance on u_2 are also collected. Figure 4b shows the validation of undesired-relay feedback responses for real-time liquid level system.



Figure 5a. Experimental setup for two interacting tank level control system

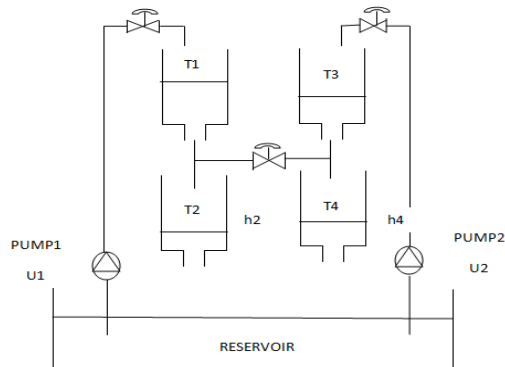


Figure 5b. Schematic diagram of coupled tanks experimental set up

6. Conclusions

A systematic approach is proposed to derive exact expressions for relay feedback responses for diagonal and interactive transfer functions in MIMO systems. The closed loop interaction transfer functions of 3x3 systems were modeled without using approximation of time delay. These results are provided in a closed form solution for the first time. These model equations are useful to back calculate the exact process model parameters. Moreover, as these interactive transfer functions carry information on interactions between inputs/outputs, these theoretical models will provide information on measuring interactions directly. This breakthrough will also help in assessing interaction measures between inputs-outputs.

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